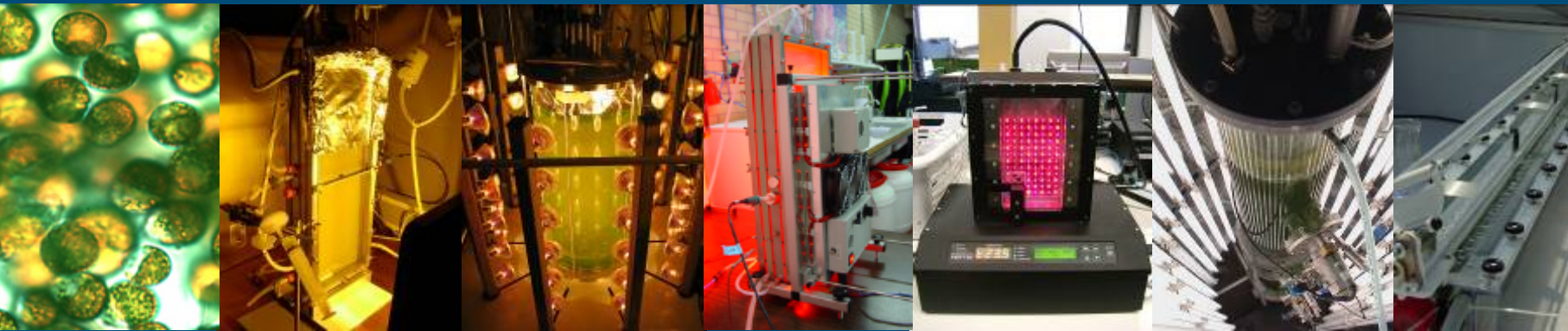


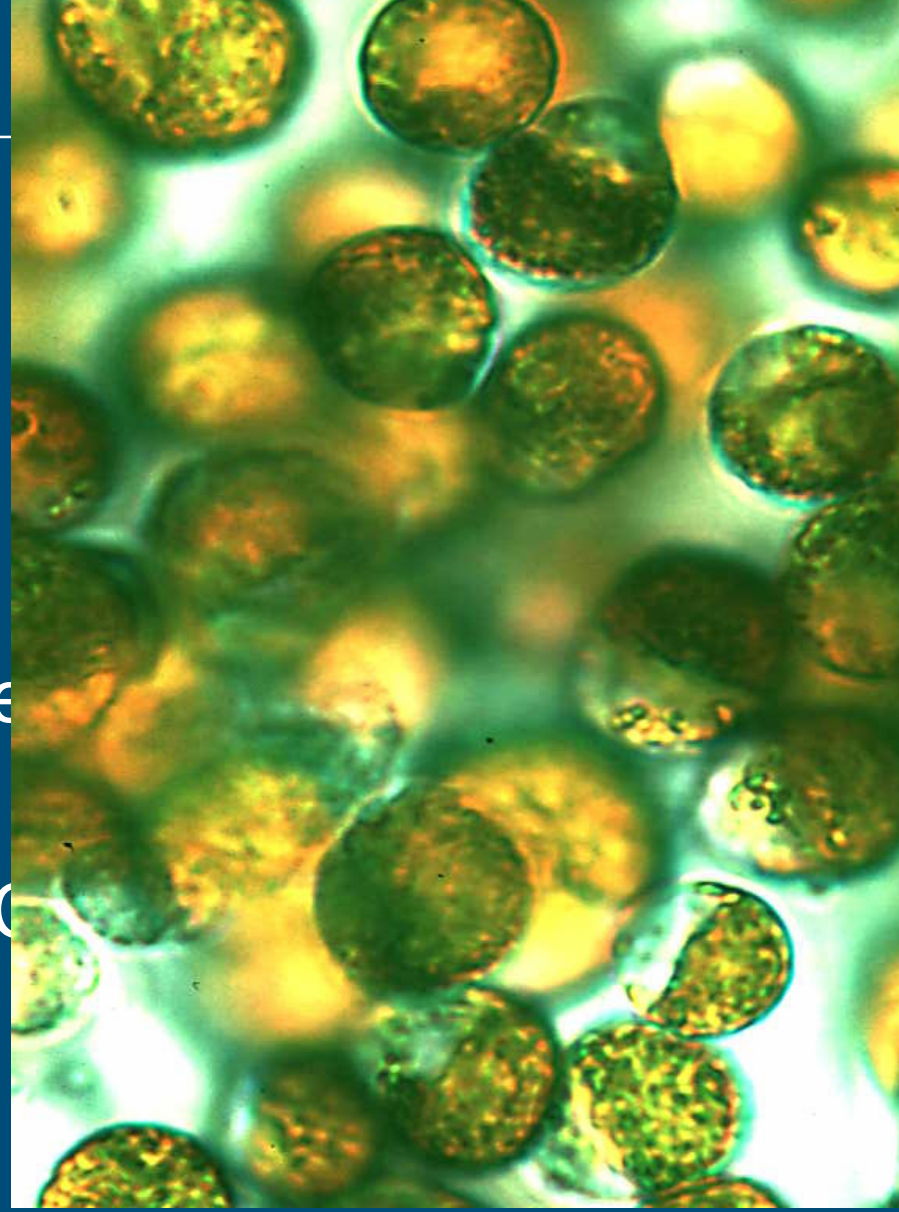
# Microalgae for production of biofuels and bulk chemicals

René H. Wijffels  
[www.algae.wur.nl](http://www.algae.wur.nl)



# Contents

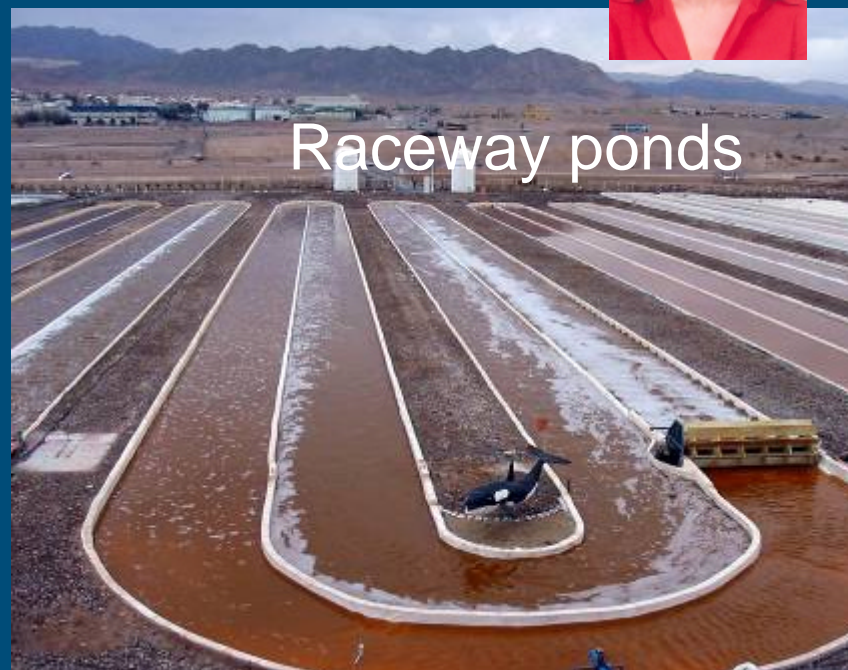
- Feasibility study
- Biorefinery of microalgae
- Research agenda
- Pilot studies: AlgaePARC







Horizontal tubes

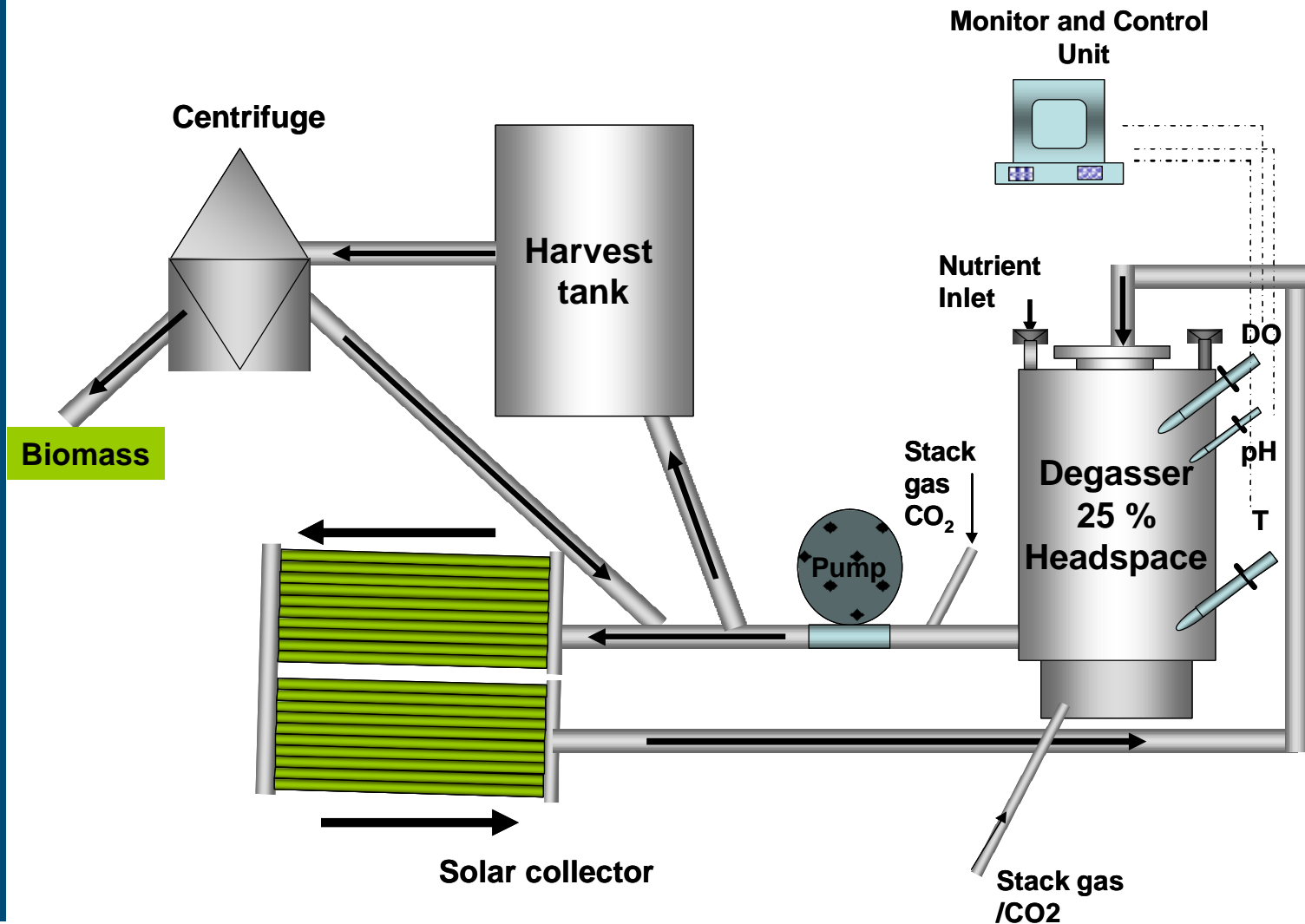


Raceway ponds



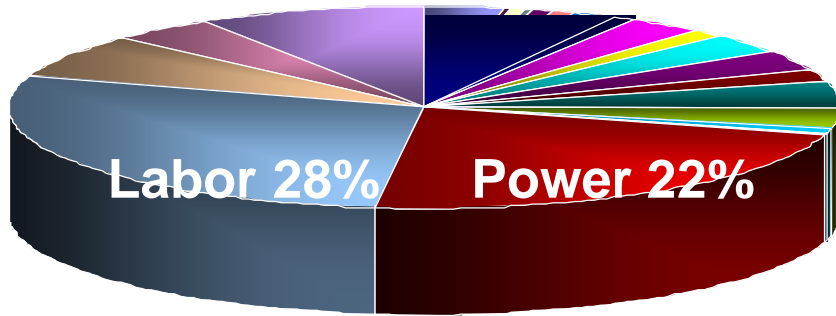
Flat panels

# Tubular reactor



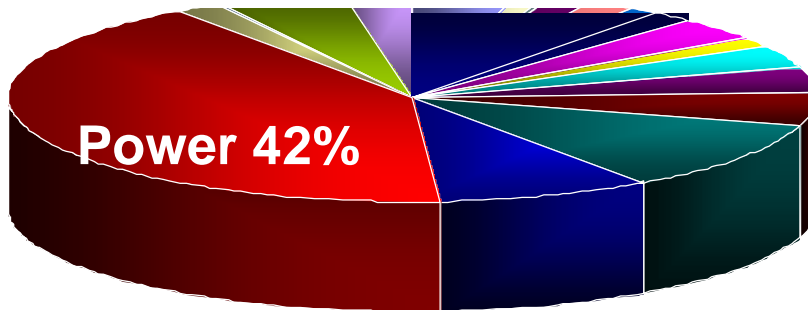
# Biomass production cost

ha



10.62 €/ kg biomass

00 ha



4.02 €/ kg biomass

89% decrease

potential

- |                                   |                                       |                            |
|-----------------------------------|---------------------------------------|----------------------------|
| Centrifuge westfalia separator AG | Centrifuge Feed Pump                  | Medium Filter Unit         |
| Medium Feed pump                  | Medium preparation tank               | Harvest broth storage tank |
| Seawater pump station             | Automatic Weighing Station with Silos | Culture circulation pump   |
| Installations costs               | Instrumentation and control           | Piping                     |
| Buildings                         | Polyethylene tubes Photobioreactor    | Culture medium             |
| Carbon dioxide                    | Media Filters                         | Air filters                |
| Power                             | Labor                                 | Payroll charges            |
| Maintenance                       | General plant overheads               |                            |

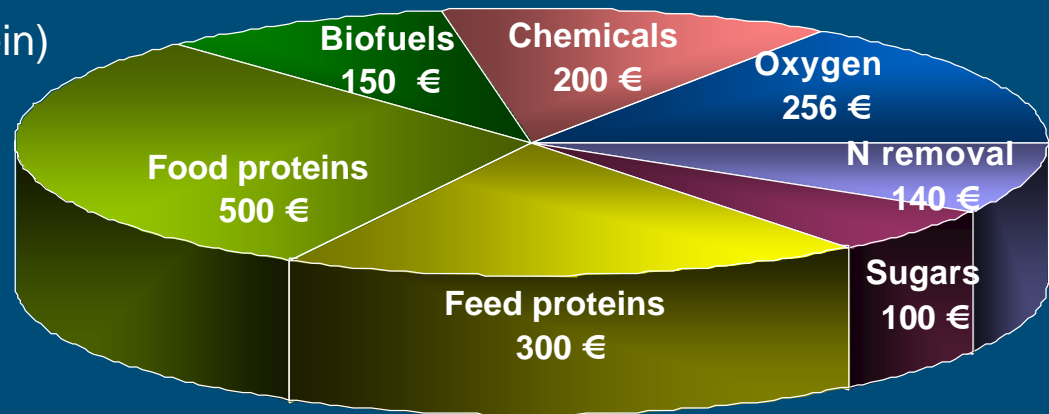
0.4 €/ kg biomass  
15 €/GJ



# Economical Viability: biorefinery of microalgae

Bulk chemicals and biofuels in 1,000 kg microalgae

- 400 kg lipids
  - 100 kg as feedstock chemical industry (2 €/kg lipids)
  - 300 kg as transport fuel (0.50 €/kg lipids)
- 500 kg proteins
  - 100 kg for food (5 €/kg protein)
  - 400 kg for feed (0.75 €/kg protein)
- 100 kg polysaccharides
  - 1 €/kg polysaccharides
- 70 kg of N removed
  - 2 €/kg nitrogen
- 1,600 kg oxygen produced
  - 0.16 €/kg oxygen
- Production costs: 0.40 €/kg biomass
- Value: 1.65 €/kg biomass





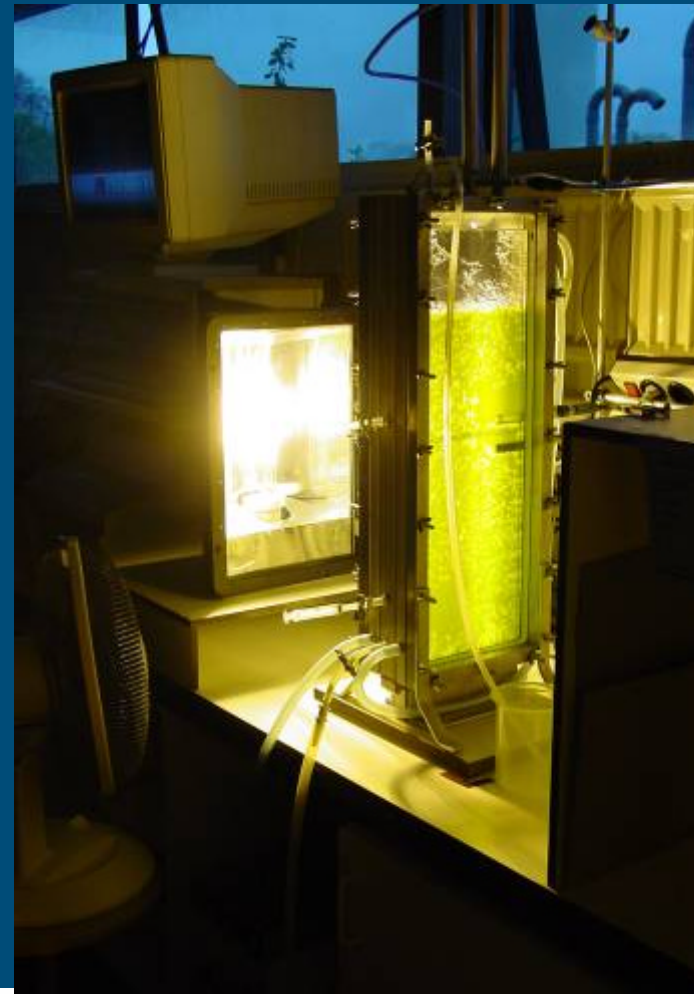
# Research programs

- Photosynthetic Cell Factories (NWO)
- Solar-H and Solar-H2, SUNBIOPATH (EU)
- Sealand Sole (Min. Agriculture, province Sealand, companies)
- SUNLIGHT (University of Ghent)
- CO<sub>2</sub> fixation (TNO)
- Reactor design (Proviron, University Huelva, Wetsus)
- AlgiCoat (Akzo, Ingrepro, Essent)
- Wetsus (15 companies)
- AlgaePARC (15 companies)



# Wageningen research agenda

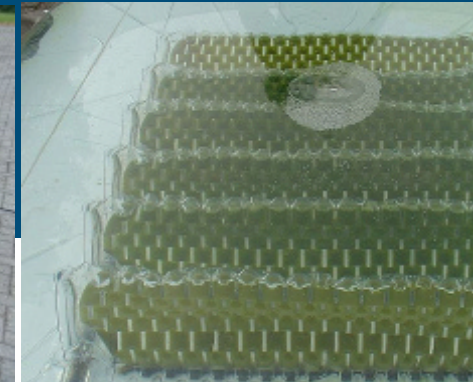
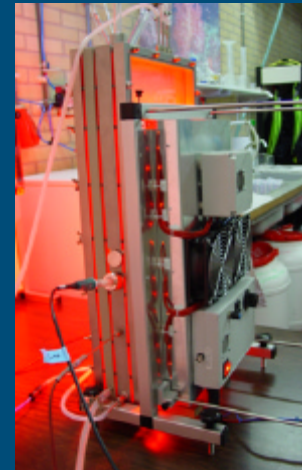
- Photobioreactor design
- O<sub>2</sub> removal and CO<sub>2</sub> supply
- Biofilms for post-treatment wastewater
- Control of primary metabolism
- Harvesting and Oil extraction
- Biorefinery
- Design scenarios





# Photobioreactor design

- Closed photobioreactors
- Maximization of photosynthetic efficiency/productivity
  - High light intensity/shading
  - High biomass density
  - Energy input
  - Shear effects
  - Growth inhibition
  - Light guides
  - Flashing light effect
  - Variations in light intensity



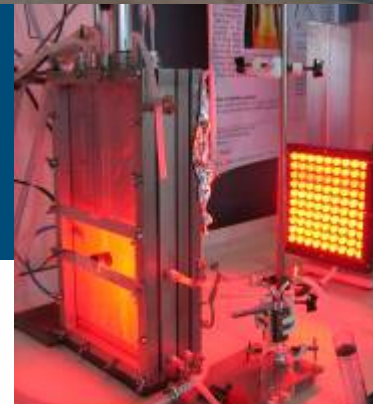
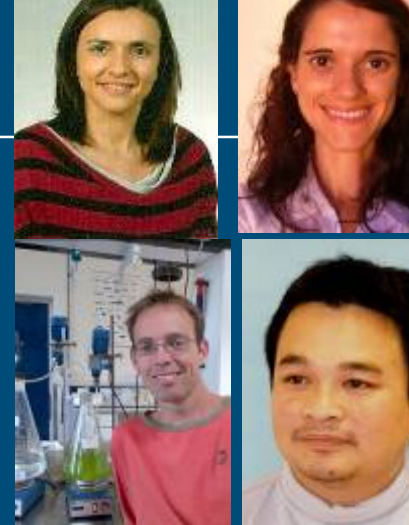
# O<sub>2</sub> removal and CO<sub>2</sub> supply

## ■ High Oxygen partial pressure inhibits photosynthesis

- Maximal tolerable O<sub>2</sub> partial pressure
- Strains more resistant to O<sub>2</sub>
- Develop new technology to remove O<sub>2</sub>

## ■ Energy efficient CO<sub>2</sub> supply

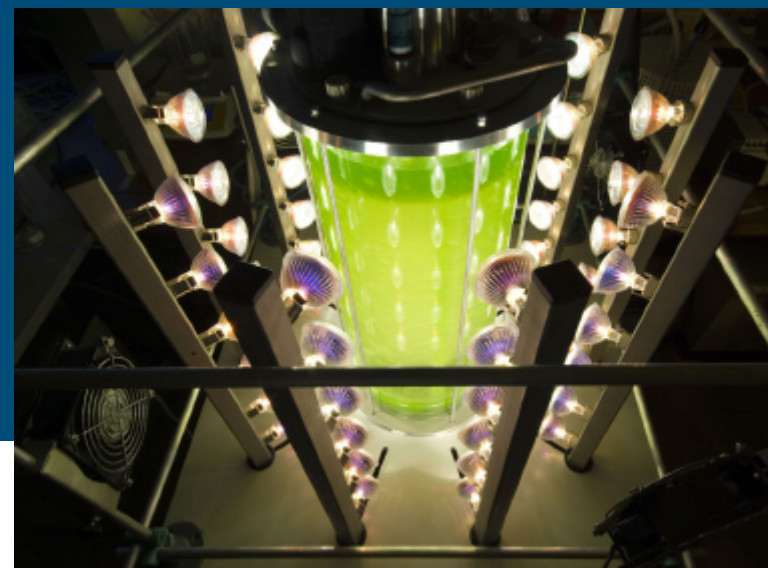
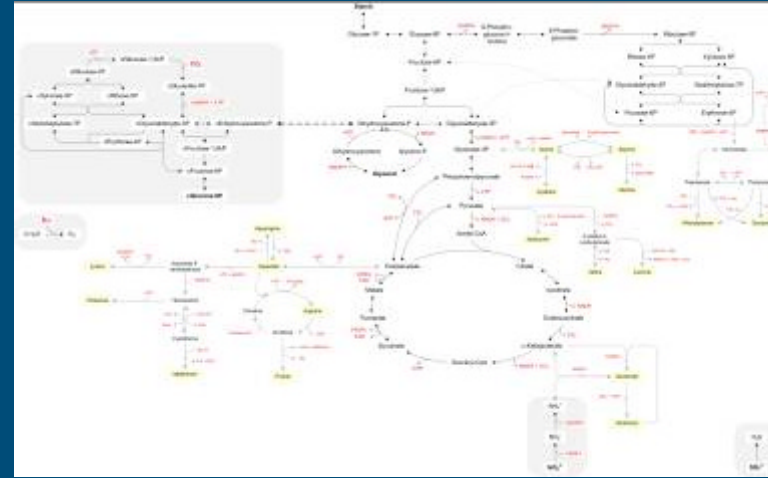
- Conditions: high pH, high salt
- Use of CO<sub>2</sub> absorbers
- Selection of lipid accumulating strains



# Control primary metabolism



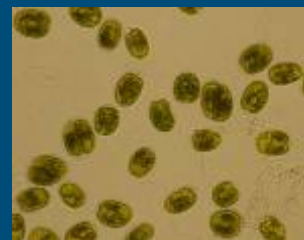
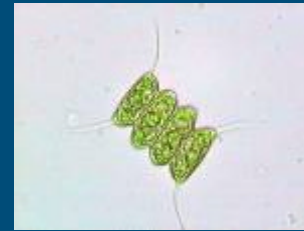
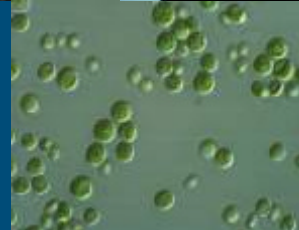
- Objective: control metabolism
  - High yield on light
  - Production of lipids
  - Production of colourants
- Metabolic network model and flux calculations to predict rates in primary metabolism
- Research reactor to apply wide range of cultivation conditions
- On-line monitoring of production and consumption rates ( $\text{CO}_2$ ,  $\text{O}_2$ , N, biomass)





# Harvesting and oil extraction

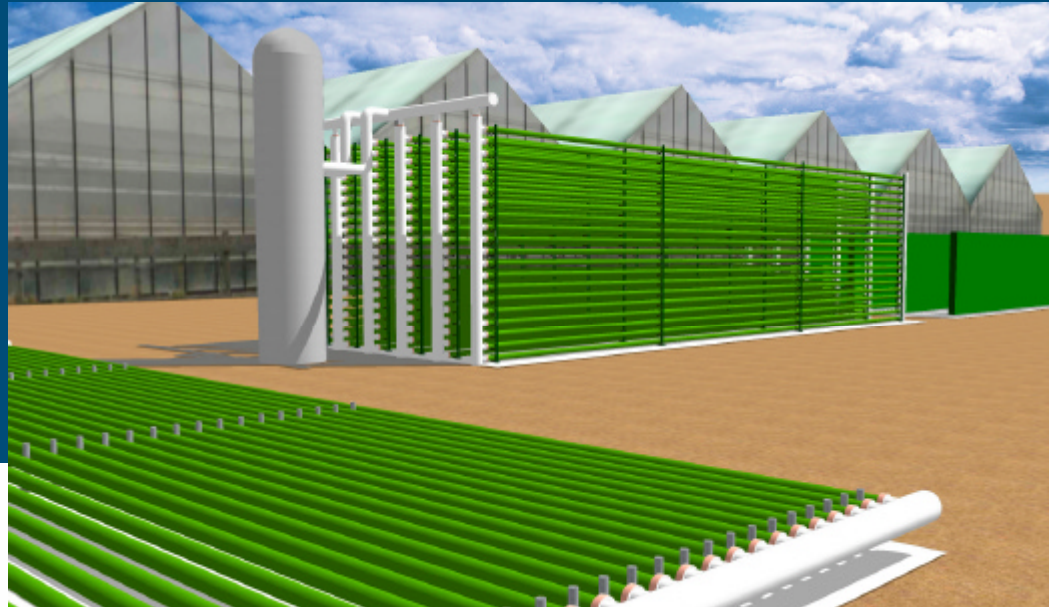
- Reduction of cost & energy demands
  - No additional chemicals
  - Ensure medium reuse
- Bio- & auto-flocculation
  - Microalgae with high lipid content
  - Characterization of algae
  - Mechanistic study
  - Kinetics of harvesting
- Milking of microalgae





# AlgaePARC: Algae Production and Research Center

- Development of a process chain
- Experience with systems
- Information for design of full scale plants
- Comparison of systems
- Comparison of strains
- Comparison of feeds (nutrients, CO<sub>2</sub>, sunlight...)
- Supply of biomass for further processing
- Further processing



# AlgaePARC

- Research plan
- 4 outdoor systems of 25 m<sup>2</sup> each
  - Open pond: reference
  - Horizontal tubular system: high light intensity, oxygen accumulation
  - Vertical tubular system: low light intensity, oxygen accumulation
  - Flat panel system: low light intensity, no oxygen accumulation
- 4-8 systems of 2.5 m<sup>2</sup>
- Specific requirements: extra systems

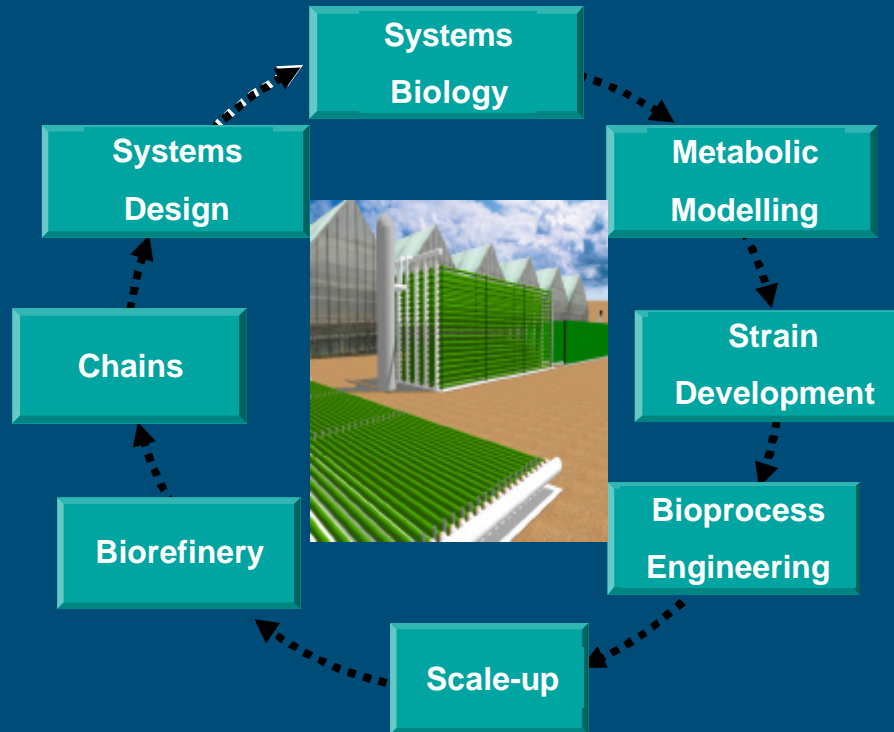


# 2.5 m<sup>2</sup> systems

- Phase between lab and pilot
- Test things where you are not sure of
- Different strains
- Different feed stocks
- Adaptations in design
- New systems
- If successful
  - To 25 m<sup>2</sup> scale
- If not successful
  - More experiments
  - Reject

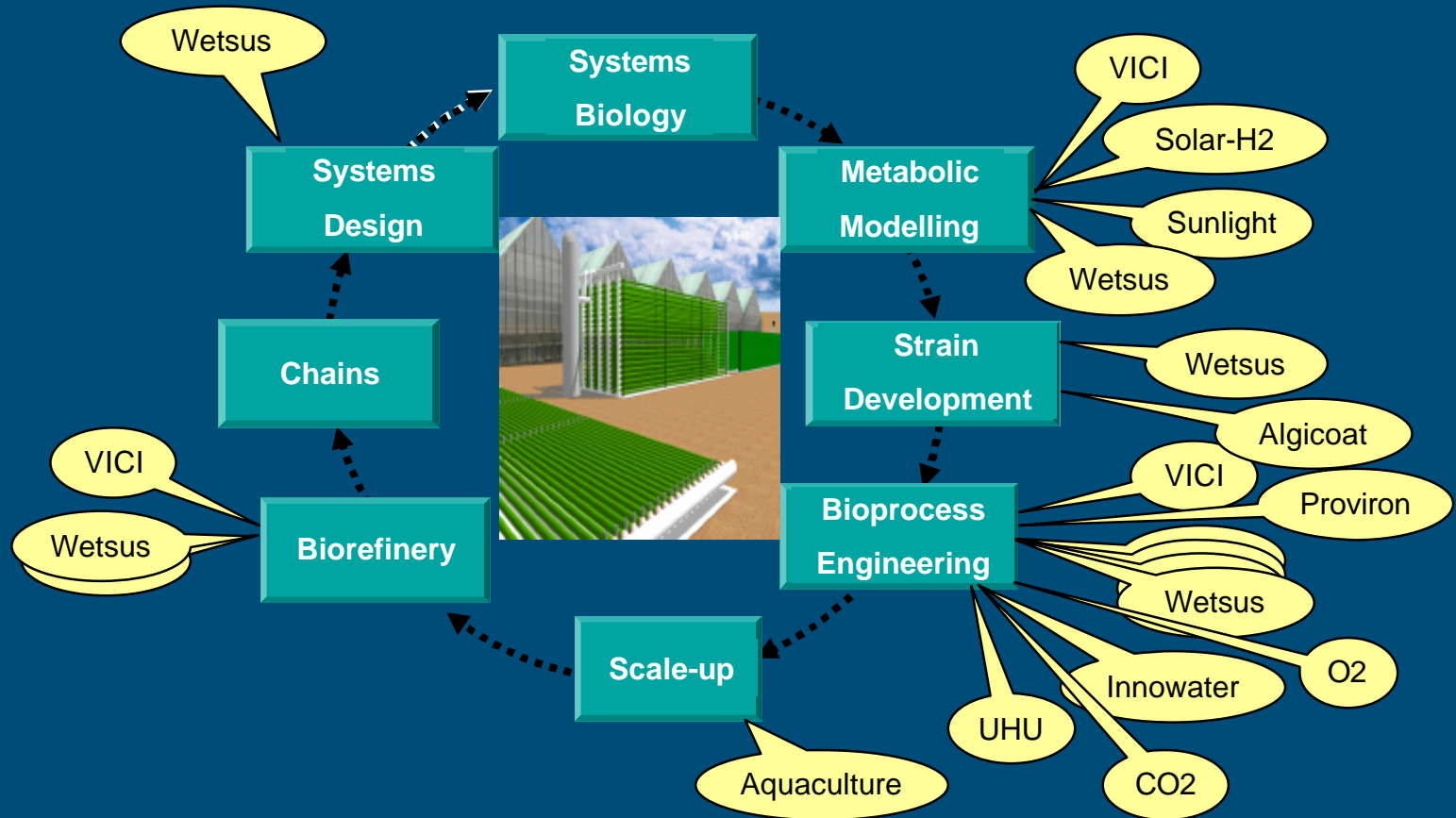


# Development of a technology

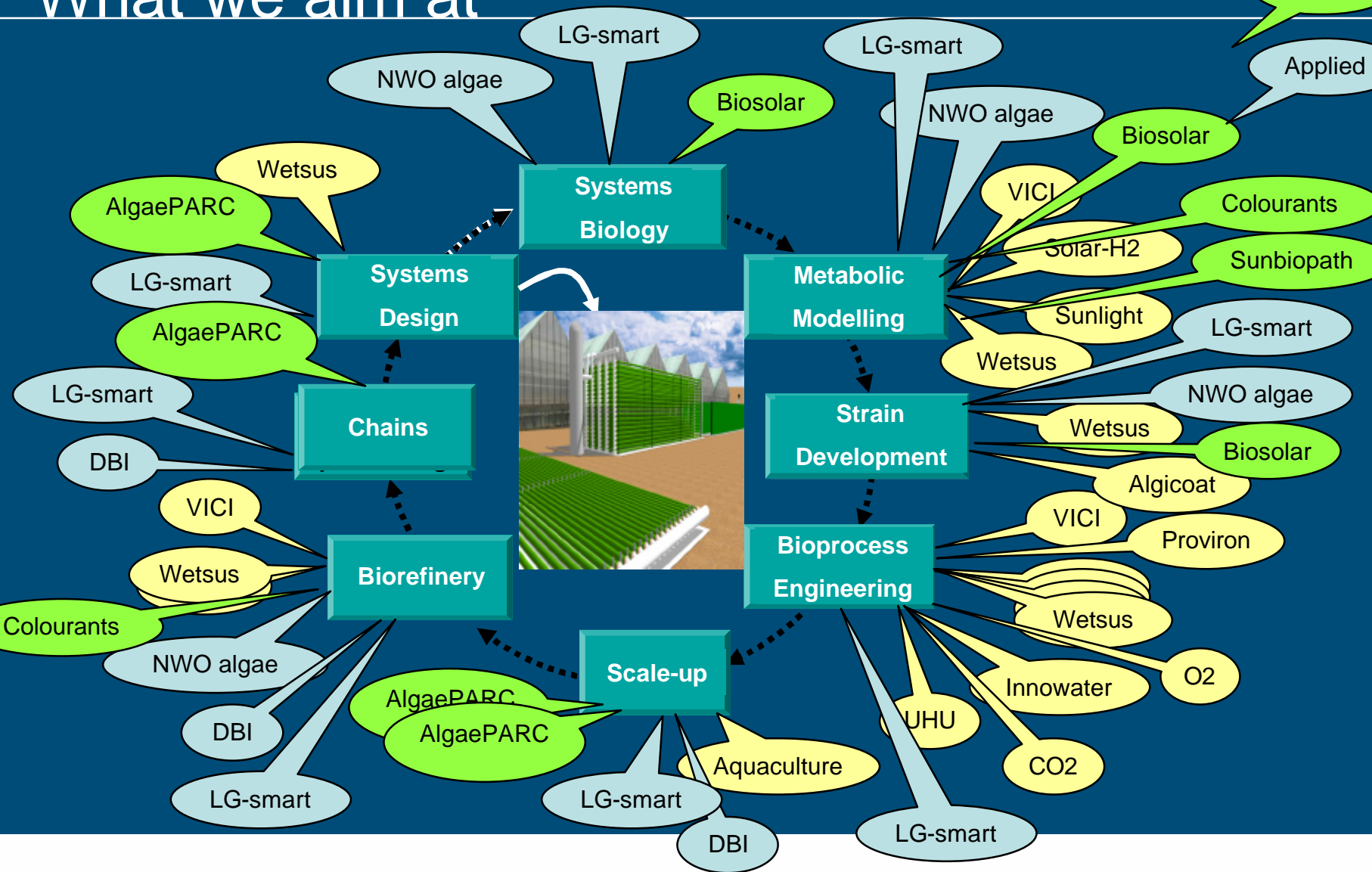




# Present research projects



# What we aim at

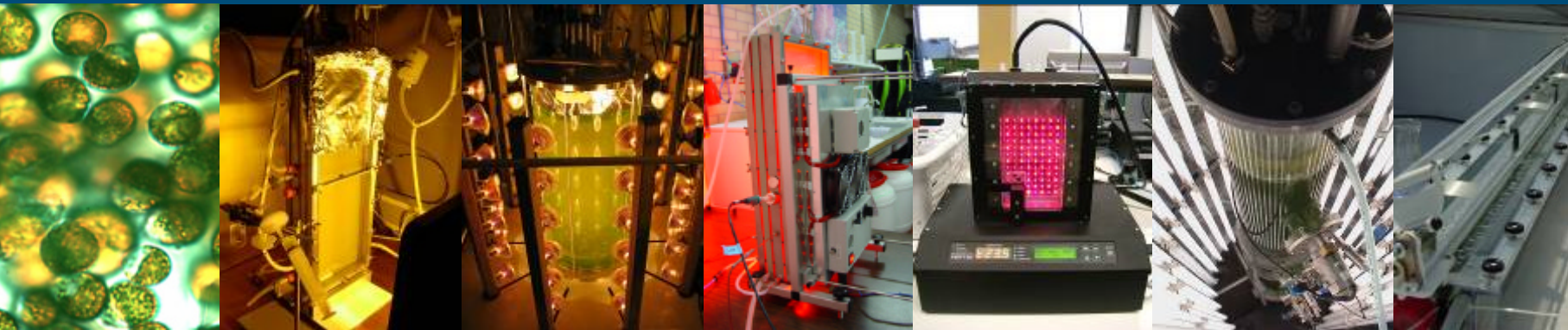


# Conclusions

- Microalgae are promising for production of bulk chemicals and biofuels
- Microalgae technology is immature
- Development of technology requires large research programs
- Combination with biorefinery important
- Join forces



[www.algae.wur.nl](http://www.algae.wur.nl)



AGROTECHNOLOGY &  
FOOD SCIENCES GROUP

WAGENINGENUR